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(54) **Acrylic copolymers and method of making the same.**

(57) The present invention provides novel acrylic block copolymers and a method of making the same by use of an iniferter as a means of promoting, controlling and terminating polymerization. The method involves mixing an iniferter with a first polymer charge of acrylic monomer polymerizable to an acrylic block, exposing the mixture to an energy source to cause the iniferter to dissociate to form free radicals, permitting the first monomer charge to polymerize, terminating the exposure, adding a second monomer charge polymerizable to a second polymer block and again exposing the mixture to produce free radicals, permitting the second monomer charge to polymerize, and terminating the second exposure.

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ACRYLIC COPOLYMERS AND METHOD OF MAKING THE SAME

Technical Field

This invention relates to acrylic block copolymers and a method of making the same.

Background Art

Various methods of producing acrylic block copolymers are known. Acrylic monomers which have been polymerized randomly by conventional thermal initiation techniques to produce polymers which may be formed into films or sheets or used as protective coatings have been known for many years. The inherent resistance of acrylic polymers to oxidation endows films, sheets and coatings of such polymers with good aging and weatherability properties. The films for the most part are clear, making them suitable for certain optical applications. Acrylic copolymers have also been widely used in adhesive applications and in particular as pressure-sensitive adhesives. The combination of monomers are, of course, diametrically different from those required of acrylic copolymers that are to be used to make films and protective coatings.

It is generally recognized that control of the polymerization to produce a block copolymer is desired in the production of useful copolymers. Control has not always been an easy task according to prior art methods.

Disclosure of the Invention

The present invention provides acrylic block copolymers and a method of making the same by utilization of an iniferter as a means of promoting, controlling and terminating polymerization of the copolymer.

The term "iniferter" refers to a chemical compound that has a combined function of being a free radical initiator, transfer agent, and terminator, the term "iniferter" being a word formed by the underlined portions of the terms identifying these functions. This term and its use in a production of block copolymers is well known, particularly because of the work of Takayuki Otsu of the Department of Applied Chemistry, Osaka City University, Osaka, Japan. This work is discussed, for example, in an article by Otsu et al entitled "Living Radical Polymerizations in Homogeneous Solution by Using Organic Sulfides as Photoiniferters", Polymer Bulletin, 7, 45-50 (1982) and an article by Otsu et al entitled "Living Mono- and Biradical Polymerizations in Homogeneous System Synthesis of AB and ABA Type Block Copolymers", Polymer Bulletin, 11, 135-142 (1984). Despite the rather detailed description of making block copolymers according to such disclosures, there is no disclosure of making the type of acrylic block copolymers herein claimed.

The present invention provides tailor-made acrylic block copolymers. The control of the polymerization provided by the iniferter technology permits "tailoring" of the acrylic block copolymer so that a wide spectrum of physical properties can be introduced. Polymerization is accomplished by sequential polymerization steps.

The acrylic block copolymers of the present invention generally have optical clarity and are resistant to oxidative and photochemical degradation. The acrylic block copolymers of the invention can be used where conventional block copolymers are employed, for example to make shaped articles, sheet materials, and the like. Many of the sheets are clear polymeric films. The films are also quite flexible without being brittle and unexpectedly craze-resistant.

Specifically, the block copolymer is made by a method which has the following steps:

(a) mixing (1) an iniferter represented by the general formula $I(T)_n$ capable upon being subjected to an appropriate energy source of forming free radicals $I(\cdot)_n$ and $nT\cdot$ wherein n is an integer of at least 2, $I\cdot$ is a highly reactive free radical capable of initiating free radical polymerization, and $T\cdot$ is a less reactive free radical which is generally much less capable of initiating free radical polymerization than $I\cdot$ but will rejoin with $I(\cdot)_n$ or a free radical polymer segment free radically polymerized with $I(\cdot)_n$ upon termination of said energy source and (2) a first monomer charge selected from the group consisting of (i) acrylic monomer polymerizable to form an acrylic polymer block having a glass transition temperature of less than 0°C and (ii) monomer polymerizable to form a thermoplastic polymer block having a glass transition temperature of at least 50°C which is free radically polymerizable in the presence of $I(\cdot)_n$ to form a first

polymer block;

(b) exposing the mixture of (a) to an energy source capable of forming free radicals $I(\cdot)_n$ and $nT\cdot$;

(c) maintaining the exposure of (b) until said first monomer charge polymerizes with $I(\cdot)_n$ to form a free radical polymer segment represented by the formula $I(B\cdot)_n$ wherein B represents said first polymer block formed of said first monomer charge;

(d) terminating said exposure whereby to cause $I(B\cdot)_n$ and $nT\cdot$ to combine to form a polymer represented by the formula $I(BT)_n$;

(e) mixing $I(BT)_n$ with a second monomer charge which is the member of the group consisting of monomer (i) and monomer (ii) which was not selected as said first monomer comprising monomer which is free radically polymerizable in the presence of $I(B\cdot)_n$ to a second polymer block;

(f) exposing $I(BT)_n$ to an energy source capable of forming free radicals $I(B\cdot)_n$ and $nT\cdot$;

(g) maintaining the exposure of (f) until said second monomer charge polymerizes with $I(B\cdot)_n$ to form a free radical block copolymer segment represented by the formula $I(BA\cdot)_n$ wherein A represents said second polymer block formed of said second monomer charge; and

(h) terminating the exposure of (f) whereby $I(BA\cdot)_n$ and $nT\cdot$ combine to form a block copolymer represented by the formula $I(BAT)_n$.

The block copolymer of the invention is an ABA type copolymer which can be represented by the general formula $I(BAT)_n$

wherein

I represents a radical derived from the free radical initiator $I\cdot$ of an iniferter of the formula $I(T)_n$ as previously defined;

T represents a radical derived from the free radical terminator $T\cdot$ of iniferter $I(T)_n$

n is an integer of at least 2;

B is a first polymer block selected from the the group consisting of (i) a polymer block having a glass transition temperature of less than 0°C and (ii) a normally thermoplastic polymer block having a glass transition temperature of at least 50°C ; and

A is a second polymer block which is the member of the group consisting of polymer block (i) and polymer block (ii) which was not selected as said first polymer block.

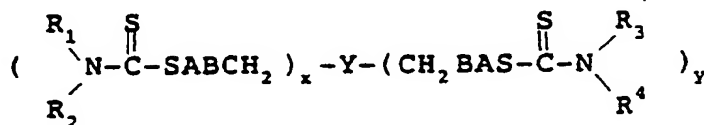
The preferred block copolymers are those wherein n is an integer of 2 to 12, most preferably 2 to 6.

The preferred weight ratio of acrylic polymer block to thermoplastic polymer block in the copolymer is from about 5:95 to 40:60, most preferably 10:90 to 30:70.

Preferred block copolymers have an elastomeric block which is formed of monomer comprising from about 75 to 100 percent by weight of at least one monomeric acrylic or methacrylic acid ester of a non-tertiary alcohol, the alcohol having from 1 to 14 carbon atoms with the average number of carbon atoms being 4 to 12. Preferred monomeric acrylic or methacrylic acid ester is selected from the group consisting of 2-butyl acrylate, isooctyl acrylate, 2-ethylhexyl acrylate, 2-methylbutyl acrylate and n-butyl acrylate.

The preferred monomeric material from which the polymer block is formed is selected from the group consisting of methyl methacrylate, polystyrylethyl methacrylate macromer, methyl methacrylate macromer, acrylic acid, acrylonitrile; isobornyl methacrylate, N-vinyl pyrrolidone, t-butyl methacrylate, isopropyl methacrylate, and mixtures thereof.

The preferred block copolymers according to the present invention include those which may be represented by the general formula



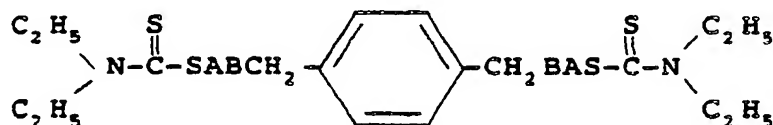
wherein

R_1 , R_2 , R_3 and R_4 are aliphatic, aromatic, or substituted aromatic moieties (preferably C_{1-4} aliphatic moieties), which can be the same or different and which do not substantially interfere with the ability of $I\cdot$ to promote free radical polymerization or with $T\cdot$ to recombine with $I\cdot$ or a polymer free radical segment including $I\cdot$;

Y is a linking group having a functionality of $x+y$ which does not substantially interfere with the ability of $I\cdot$ to promote free radical polymerization or the ability of $T\cdot$ to recombine with $I\cdot$ or a polymer free radical segment including $I\cdot$; and

x and y are each integers of at least 1 and the sum of $x+y$ is not more than 12.

The most preferred block copolymers according to the invention are those represented by the formula



The most preferred iniferters for producing the ABA block copolymers according to the present invention are selected from the group consisting of xylylene bis (N,N-diethyl dithiocarbamate) and xylylene bis (N-carbazoyl dithiocarbamate).

Best Mode for Carrying Out The Invention

The acrylic monomer of the elastomeric block as previously mentioned, is a monomeric acrylic or methacrylic acid ester of a non-tertiary alcohol, said alcohol having from 1 to 14 carbon atoms with the average number of carbon atoms being about 4-12. Examples of such monomers include the esters of acrylic acid or methacrylic acid with non-tertiary alkyl alcohols such as 1-butanol, 1-pentanol, 2-pentanol, 3-pentanol, 2-methyl-1-butanol, 1-methyl-1-butanol, 1-methyl-1-pentanol, 2-methyl-1-pentanol, 3-methyl-1-pentanol, 2-ethyl-1-butanol, 3,5,5-trimethyl-1-hexanol, 2-ethyl hexanol, 3-heptanol, 2-octanol, 1-decanol, 1-dodecanol, and the like. Such monomeric acrylic or methacrylic esters are known in the art and many are commercially available.

The elastomeric block may include as a comonomer a macromolecular monomer, sometimes referred to as a "macromer". Such a monomer may also be included in the thermoplastic polymer block as a comonomer. Such a monomer is a polymeric material having a copolymerizable vinyl group with which the acrylic monomer and other monomers (if more than one is used) will copolymerize under the polymerization conditions.

The vinyl-terminated polymeric monomers useful in the present invention are known and may be prepared by the method disclosed by Husman et al, U.S. Pat. No. 4,554,324 describes the preparation of the vinyl-terminated polymeric monomers. The most preferred macromolecular monomers include polystyrylethyl methacrylate macromer and polymethyl methacrylate macromer.

According to Husman, such monomers are known and may be prepared by the method disclosed by Milkovich et al as described U.S. Pat. Nos. 3,786,116 and 3,842,059. As disclosed therein, vinyl-terminated polymeric monomer is prepared by anionic polymerization of a polymerizable monomer to form a living polymer. Such monomers include those having an olefinic group, such as the vinyl-containing compounds. Living polymers are conveniently prepared by contacting the monomer with an alkali metal hydrocarbon of alkoxide salt in the presence of an inert organic diluent which does not participate in or interfere with the polymerization process. Monomers which are susceptible to anionic polymerization are well known. Illustrative species include vinyl aromatic compounds such as styrene, alpha-methylstyrene, vinyltoluene and its isomers. Other monomers susceptible to anionic polymerization are also useful.

The initiators for anionic polymerization may be any of the alkali metal hydrocarbons of alkoxide salts which produce a mono-functional living polymer, i.e., only one end of the polymer contains a reactive ion. Such initiators include the hydrocarbons of lithium, sodium or potassium, for example, having an alkyl radical containing up to 20 carbon atoms or more, and preferably up to 8 carbon atoms. Illustrative alkali metal hydrocarbons include ethyllithium, propyllithium, butylpotassium, octyl-potassium, phenyllithium, ethyllithium, butyllithium, sec-butyllithium, isobutyllithium, tertbutyllithium and 2-ethylhexyllithium. Sec-butyllithium is the preferred initiator.

The inert organic diluent utilized to facilitate heat transfer and adequate mixing of the initiator and monomer preferably is a hydrocarbon or an ether. Useful diluents include saturated aliphatic and cycloaliphatic hydrocarbons such as hexane, heptane, octane, cyclohexane and the like. In addition, aliphatic and cyclic ether solvents may be used, for example, dimethyl ether, diethyl ether, and tetrahydrofuran.

The amount of initiator usually dictates the molecular weight of the living polymer. If a small portion of initiator is used, with respect to the amount of monomer, the molecular weight of the living polymer will generally be larger than if a large portion of initiator is used. It is generally advisable to add initiator dropwise to the monomer until the persistence of the characteristic color of the organic anion is observed, then the calculated amount of the initiator is added for the molecular weight desired. The preliminary

dropwise addition serves to destroy contaminants and thus permits better control of the polymerization. Generally, the initiator concentration can vary from about 0.01 to about 0.1 mole of active alkali metal per mole of monomer, or higher. Preferably, the concentration of the initiator will be from about 0.01 to about 0.04 mole of active alkali metal per mole of monomer.

5 The temperature of the polymerization will depend upon the monomer. Generally, the reaction can be carried out at a temperature ranging from about -100° C. up to about 100° C.

The anionic polymerization must be carried out under controlled conditions so as to exclude substances which destroy the initiator or living anion. Water and oxygen must be excluded. The polymerization therefore is carried out under anhydrous conditions in an inert atmosphere such as nitrogen, helium or
10 argon.

The living polymers may be terminated in several ways. It is important, however, that conditions be selected to provide a quantitative termination free from side reactions. Under certain conditions the living polymeric anion may be allowed to react directly with halogen-containing terminating agents to produce, for example, vinyl-terminated polymeric monomers. In many cases, however, the polymeric anion is highly
15 reactive and non-selective in its reaction with the terminating agent. In addition to displacement of the halogen atom, it may abstract hydrogen atoms or react with other functional groups present, including the vinyl group itself. This results in polymer chains which are non-functional or of unwanted functionality and molecular weight. Occasionally, under these conditions, a vinyl-terminated polymer may be attached by living anion and its functionality destroyed.

20 One means for overcoming the foregoing problem is to render the living anion less reactive, thus less susceptible to side reactions, by "capping" with a less reactive end group prior to actual termination. Examples of suitable "capping agents" include lower alkylene oxides such as ethylene and propylene oxide, and 1,1-diphenyl-ethylene, etc. A preferred capping agent is an alkylene oxide, such as ethylene oxide. The capping agent reacts with the living polymer, destroying its oxirane ring. The alkoxide anion then
25 displaces the halogen atom of the terminating agent selectively, leaving the vinyl group intact.

The capping reaction is carried out quite simply, as in the case of the terminating reaction, by adding the capping reactant to the living polymer at the polymerization temperature. The reaction occurs immediately. As in the case of the termination reaction, a slight molar excess of the capping reactant with respect to the amount of initiator may be used. The reaction occurs on a mole for mole basis. This reaction
30 is described in Milkovich, U.S. Pat. No. 3,842,059. According to U.S. Pat. No. 3,842,059, reaction with the terminating agent provides the desired vinyl-terminated polymeric monomer.

A second method of termination, also useful for synthesis of the vinyl-terminated polymeric monomers, involves capping the living anion performed as described previously, and the protonating the alkoxide ion to produce a hydroxyl-terminated polymer. The hydroxyl group is then allowed to react with a terminating
35 agent containing an isocyanate group (instead of a halogen atom) to produce the vinyl termination. Suitable terminating agents for this reaction are isocyanato alkyl acrylates and methacrylates having 1 to 4 carbon atoms in the alkyl group. The hydroxyl and isocyanato groups react to form a urethane linkage between the polymeric segment and the "monomeric" end group. Intermediate protonation of the alkoxide is necessary to prevent unwanted side reactions upon termination.

40 Although U.S. Pat. No. 3,786,116 teaches that the molecular weight distribution of the polymer chains of the vinyl-terminated polymeric monomer prior to copolymerization must be narrow, i.e., less than 1.1 polydispersity, it has been found that useful psa compositions according to the present invention may employ polymeric monomer having a polydispersity of up to about 3 without deleterious effects on the adhesive properties. These broader molecular weight distributions may be obtained by known variations in
45 temperature of polymerization and the lithium alkali initiator used.

The vinyl-terminated polymeric monomers useful in the present invention may also be prepared by free-radical polymerization (rather than anionic polymerization). Known methods can be used to prepare semi-telechelic polymers using thermal free-radical initiators. An illustrative method is described in Y. Yamashita, K. Ito, H. Mizuno and H. Okada, Polymer Journal 14, 255-260 (1982) and K. Ito, N. Usami, and Y.
50 Yamashita, Macromolecules 13,216-221 (1980). These functional polymers can then be converted into vinyl-terminated monomers using standard condensation chemistry, ring opening reactions, etc. Specifically, carboxylic-acid terminated low molecular weight polystyrene can be prepared using 4,4'-azobis-(4-cyanovaleric acid) as an initiator and an acid-containing chain transfer agent such as HS-CH₂-COOH. The semi-telechelic polystyrene can then be vinyl terminated via, for example, ring opening of glycidyl
55 methacrylate. These vinyl-terminated polymers have a high polydispersity.

It should be understood that minor amounts of the monomer forming the B block, the monomer forming the A block, or both may be present as a homopolymer in the copolymer thermoplastic composition of the invention. Such minor amounts of homopolymer may be produced in an unwanted side reaction during

polymerization of the copolymer. Such amounts will typically be less than 10 parts by weight of all homopolymer based upon 100 parts by weight of copolymer.

The copolymerization of the low T_g acrylic monomer, and the high T_g monomer to produce the thermoplastic block copolymer is by step-wise free radical polymerization. The low T_g acrylic monomer is dissolved in a suitable inert solvent, if needed, and polymerized by a first free radical polymerization utilizing a suitable iniferter as a free radical initiator source. Generally, from about 0.01 to about 5 percent by weight of iniferter based upon the total weight of polymerizable composition is used.

The iniferter is caused to dissociate to form free radicals by exposure to an appropriate energy source. The preferred iniferter is one which will dissociate upon exposure to a radiant energy source, most preferably an ultraviolet radiant energy source. Upon exposure to the energy source, the iniferter dissociates to form free radicals which promote free radical polymerization. Upon completion of the free radical polymerization of the first monomer charge, e.g., the acrylic low T_g monomer, the energy source is discontinued to permit the free radically polymerized segments to recombine with the terminator portion of the iniferter to form polymer segments. The second monomer charge is then introduced, which for example is polymerizable to the high T_g thermoplastic polymer block, and the new mixture is exposed to the energy source to cause dissociation of the terminator radical and free radical polymerization of the second monomer charge onto the first polymer segment, that now being the initiator of the second free radical polymerization. Upon completion of polymerization of the second monomer charge, the energy source is terminated and the terminator portion of the iniferter recombines with the high T_g thermoplastic polymer block to provide a block copolymer.

The particular energy source and its intensity are selected to result in dissociation of the iniferter to free radicals. When employing a photoiniferter which will dissociate upon exposure to ultraviolet light radiation, an ultraviolet light source is utilized. The intensity and rate of irradiation are chosen to advance the polymerization at a reasonable rate without deleteriously affecting the polymer segment being produced. An ultraviolet light source having a wave length on the order of 300 to 400 nm spaced approximately 10 cm from the reactants to provide an exposure of 2 mw per square centimeter has been found to produce suitable results. Reaction times on the order of 2 to 50 hours have been found to be typical, depending upon the intensity of the radiation, with faster reaction times being observed at greater intensities.

The reactants and any solvent employed are charged into an energy source-transparent vessel and therein subjected to the energy source. If the energy source is ultraviolet light radiation, a suitable ultraviolet light-transparent vessel is utilized.

The reaction is preferably conducted in a vessel with agitation to permit uniform exposure of the reactants to the energy source. While most of the reactions have been conducted by employing a batch process, it is possible to utilize the same technology in a continuous polymerization operation.

The reaction mixture may include a suitable inert solvent but it is not necessary since some of the monomeric materials are liquid themselves and may thus be charged into the reaction vessel without utilization of a solvent.

The solvent, if utilized in the free radical polymerization, may be any substance which is liquid in a temperature range of about -10°C to about 50°C , is substantially transparent to the energy source employed to permit dissociation of the iniferter to form free radicals, is inert to the reactants and product, and will not otherwise adversely affect the reaction. Suitable solvents include water, alkyl acetates such as ethyl acetate, alkanes such as hexane or heptane, and alcohols such as methyl alcohol, ethanol, isopropyl alcohol, and mixtures of one or more of these. Other solvent systems are useful. The amount of solvent is generally about 30 to 80 percent by weight based on the total weight of the reactants and solvent. In addition to solution polymerization herein described, the copolymerization may be carried out by other well known techniques such as suspension, emulsion and bulk polymerization.

The copolymer may, when necessary or desirable, be blended with a compatible modifier in order to optimize physical properties. The use of such modifiers is common in the art. For example, it may be desirable to include such materials as pigments, fillers, stabilizers, or various polymeric additives.

The copolymers prepared in accordance with the present invention are easily shaped by conventional techniques and equipment to produce shaped articles, sheet goods, or other useful shapes.

It should be noted that, while the polymers of the present invention have improved toughness without subsequent cross-linking, if necessary, further solvent resistance and resistance to photochemical or oxidative forces may be obtained by cross-linking by employing radiant energy or chemical procedures.

Examples

The following detailed description includes exemplary preparations of ABA acrylic block copolymers in accordance with the invention. All parts and percentages in the examples are by weight unless otherwise specified.

5

Definitions of Terms

The number-average molecular weight (M_n), and weight-average molecular weight (M_w), are well known mathematical descriptions of the molecular weight distribution of a polymer sample.

Each of the foregoing is a well known term used by polymer chemists and others. Further explanation of the derivation of these terms may be found in Experimental Methods in Polymer Chemistry, Wiley and Sons, 1981, Chapter 3 entitled "Molecular Weight Averages", pages 57-61.

The block copolymers of the present invention are described in a short-hand way depending upon the monomer forming each block. For example, MMA-b-BA-b-MMA refers to a copolymer having block ("b") of polymerized methyl methacrylate ("MMA") and a block of polymerized butyl acrylate ("BA"). For example, MMA-b-BA-b-MMA refers to an ABA block copolymer having two A (polymethyl methacrylate) blocks and a single B midblock (poly-butyl acrylate).

20

Test Methods

The test methods used to evaluate the block copolymers of the examples are industry standard tests. The test methods which characterize the polymers of this invention are those which demonstrate its molecular architecture. The gel permeation chromatography (GPC), inherent viscosity (I.V.) modulus, percent elongation, and tensile strength measurement results have been obtained. The standard tests are described in detail in various publications of the American Society for Testing and Materials (ASTM), Philadelphia, Pa. The standard test methods are described in detail below. The reference source of each of the standard test methods is also given.

35

Gel Permeation Chromatography

The characterization of the molecular weight distribution of the polymers has been by conventional gel permeation chromatography (GPC).

A Hewlett-Packard Model 1084B, high performance liquid chromatograph equipped with Styragel™ columns was used. The system was calibrated using polystyrene standards. All molecular weight averages are polystyrene equivalent molecular weights. The molecular weight averages and polydispersities were calculated according to accepted practices. GPC test methods are further explained in "Modern Size Exclusion Liquid Chromatography" Practice of Gel Permeation Chromatography, John Wiley and Sons, 1979.

45

Modulus - Elongation- Tensile Measurements

The mechanical properties of the toughened, non-brittle, thermoplastic films formed from the copolymers of this invention were measured according to the procedures established by the American Standard Test Methods (ASTM) which can be found under the designations: D-412-83, "Rubber Properties in Tension" and D 638M-84, "Tensile Properties of Plastics".

Preparation of films for test purpose: Films were cast from solution upon a substrate which permitted subjecting the film to 16 hours of drying in a vacuum oven at 50°C. The film thus formed was cut to standard dumbbell shapes to provide test samples for insertion in the jaws of an Instron™ tensile test instrument where it was tested under ambient conditions in a testing room controlled at 23°C and a humidity of 50%.

The prescribed dumbbell-shaped specimens were stretched at a constant rate to the breaking point.

The tensile strength at break was recorded. The elongation was expressed as a percentage of the original length. The modulus (Stiffness) and tensile strength were calculated based on the following formulae where "force" is expressed in Newtons (N), linear dimensions in meters and the modulus and tensile units are expressed as megaPascals (MPa).

$$\text{Tensile} = \frac{\text{Force}}{\text{Width} \times \text{Thickness}}$$

$$\text{Modulus} = \frac{\text{Force} \times \text{Initial Length}}{\text{Width} \times \text{Thickness} \times \text{Final Length}}$$

$$\begin{aligned} \% \text{ Elongation} \\ \text{at break} &= \frac{\text{final length} - \text{original length}}{\text{original length}} \times 100 \end{aligned}$$

Inherent Viscosity Measurement

The inherent viscosity is measured by conventional means using a Cannon-Fenske #50 viscometer in a water bath controlled at 25 °C to measure the flow time of 10 ml of a polymer solution (0.2 g per deciliter polymer in methyl ethyl ketone). The examples and comparative examples were run under identical conditions. It is the comparative values which are significant and absolute figures are not required.

Example 1

MMA-b-BA-b-MMA

A cylindrical reaction bottle was charged with 36 grams of butyl acrylate (BA), 0.2 grams of xylylene bis (N,N-diethyl-dithiocarbamate) (XDC) and 21.3 grams of ethyl acetate. The mixture was purged with nitrogen for 10 minutes before sealing and placing the sealed bottle in a roller mechanism. The rotating, sealed bottle was exposed for 39 hours to ultraviolet radiation from General Electric 15 watt black light lamp. At this point, the ultraviolet source was turned off, the reaction bottle was unsealed then 65.6 grams of methyl methacrylate (MMA) and 21.3 grams of ethyl acetate were added to the polymerized butyl acrylate. Purging for 10 minutes with nitrogen followed before the reaction bottle was re-sealed and placed in the roller mechanism for further exposure to ultraviolet radiation which continued for 66 hours. The resulting triblock copolymer solution was removed. The composition of the resultant polymer was determined by NMR spectroscopic analysis. A thin film was cast and dried to be subjected to mechanical tests. The results of these tests are reported in Table I, Example 1.

Examples 2, 3, 4 and 5

The procedure of Example 1 was followed. The same monomers were charged but at different ratios and the exposure to ultraviolet and the amount of photoiniferters was varied. The resulting range of molecular weights and inherent viscosities show how modulus, elongation and tensile performance of the toughened thermoplastic film can be altered.

Table I

Segmented Triblock Copolymers MMA-b-BA-b-MMA						
Ex.	Composition BA/MMA	Molecular Weight	I.V. (dl/g)	Performance Data		
				Modulus (MPa)	Elong. (%)	Tensile (MPa)
1	35/65	167,790	0.71	1,054	4	29.1
2	29/71	182,345	--	939	5	30.5
3	31/69	100,889	--	1,239	7	38.8
4	38/62	109,188	0.47	738	17	24.2
5	30/70	94,600	0.48	659	21	25.0

Examples 6, 7, 8 and 9

The preparation of these segmented triblock copolymers of 2-butyl acrylate (2-BA) and methyl methacrylate (MMA) were carried out by the procedure described in Example 1. The photoiniferter was xylylene bis (N,N diethyl-dithiocarbamate) (XDC). The exposure to ultraviolet radiation was in the same range. The results of the mechanical tests performed on dried thin films of these copolymers cast from solvent are reported in Table II.

Table II

Segmented Triblock Copolymers MMA-b-2-BA-b-MMA						
Ex.	2-BA/MMA	Molecular Weight	I.V. (dl/g)	Performance Data		
				Modulus (MPa)	Elong. (%)	Tensile (MPa)
6	38/62	119,889	0.55	756	25	25.8
7	28/72	111,564	0.53	1,080	29	24.5
8	35/65	60,208	0.75	710	21	25.8
9	32/68	70,785	0.54	842	10	29.9

Comparative Examples of Random Thermoplastic Polymer by Thermal TechniqueBA/MMAExample A

A solution of monomers was prepared by charging 10 grams of butyl acrylate (BA) monomer; 90 grams of methyl methacrylate (MMA) monomer; 0.3 grams of 2,2'-azobis (isobutyronitrile) initiator (commercially available as VAZO 64™) and 100 grams of ethyl acetate solvent to a reactor bottle. The charged bottle was purged with nitrogen to remove oxygen, then sealed and placed in a rotating water bath where it was tumbled for 24 hours at 60°C to complete conversion measured by nuclear magnetic resonance (NMR) technique. The resulting random copolymer solution was removed from the reaction bottle. A thin film was

cast and dried then subjected to mechanical tests. The results of these tests are reported to Table III, Example A.

Examples B and C

The preparation of these random copolymers by conventional thermal techniques was carried out using the same procedure used to prepare Example A. The amount of the soft butyl acrylate (BA) monomer was raised from initial 10 parts to 50 parts with the corresponding decrease from 90 parts of methyl methacrylate (MMA) to 50 parts. The molecular weight ranges and the inherent viscosities varied due to the conditions of polymerization.

Table III

Non-Segmented -- Random Copolymers						
Ex.	Composition BA/MMA	Molecular Weight	I.V. (dl/g)	Performance Data		
				Modulus (MPa)	Elong. (%)	Tensile (MPa)
A	10/90	147,583	0.61	1,657	3	60.1
B	30/70	132,001	0.69	1,136	2.7	37.4
C	50/50	108,375	0.76	439	183	11.8

Table III shows the advantages of segmented copolymers of Tables I and II over the random, non-segmented, otherwise similar butyl acrylate (BA) and methyl methacrylate (MMA) copolymers. For example, when the random 30:70 BA:MMA of Table III is compared to the lower molecular weight (111,564) example 28:72 of Table II its elongation of only 2.7% is in sharp contrast to almost 30% elongation of triblock MMA/2-BA/MMA of the invention. This clearly demonstrates the effectiveness of imparting flexibility by having BA contributing its rubber properties in block-form which does not significantly reduce the modulus.

While this invention has been described in connection with specific embodiments, it should be understood that it is capable of further modification. The claims herein are intended to cover those variations which one skilled in the art would recognize as the chemical equivalent of what has been described here.

Claims

1. A copolymer characterized by the general formula $I(BAT)_n$

wherein

I represents the free radical initiator portion of an iniferter of the formula $I(T)_n$

T represents the termination portion of said iniferter;

n is an integer of at least 2;

B represents a first polymer block selected from the group consisting of (i) an elastic acrylic polymer block having a glass transition temperatures of less than 0°C; and (ii) a normally thermoplastic polymer block having a glass transition temperature of at least 50°C; and

A represents a second polymer block selected from the group consisting of polymer block (i) and polymer block (ii) which was not selected as said first polymer block

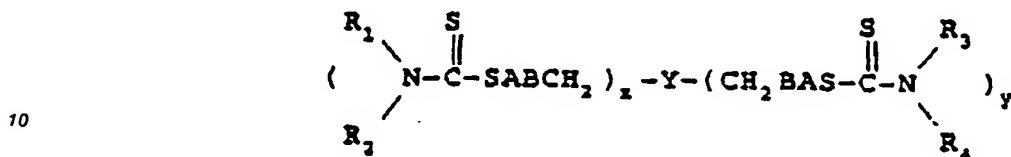
the weight ratio of said acrylic polymer block to said thermoplastic block in said block copolymer being from about 5:95 to 40:60.

2. The copolymer of claim 1 further characterized by said elastic acrylic polymer block being formed of a monomer comprising at least one monomeric acrylic or methacrylic acid ester of a non-tertiary alcohol, said alcohol having from 1 to 14 carbon atoms with the average number of carbon atoms being about 4 to 12.

3. The copolymer of claim 2 further characterized by the selection of said monomeric acrylic or methacrylic acid ester from the group consisting of 2-butyl acrylate, isooctyl acrylate, 2-ethylhexyl acrylate, 2-methylbutyl acrylate, and N-butyl acrylate.

4. The copolymer of claim 1 further characterized by the formation of said thermoplastic polymer block of monomer selected from the group consisting of methyl methacrylate, polystyrylethyl methacrylate macromer, methyl methacrylate macromer, acrylic acid, acrylonitrile, isobornyl methacrylate, N-vinyl pyrrolidone, t-butyl methacrylate, isopropyl methacrylate and mixtures thereof.

5. The copolymer of claim 1 represented by the formula



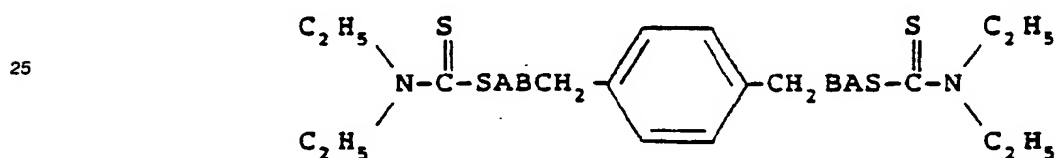
wherein

15 R_1 , R_2 , R_3 , and R_4 are aliphatic or aromatic moieties which can be the same or different and which do not substantially interfere with the ability of I^\bullet to promote free radical polymerization or with the ability of T^\bullet to recombine with I^\bullet or a polymer free radical segment including I^\bullet ;

Y is a linking group having a functionality of $x + y$ which does not substantially interfere with the ability of I^\bullet to promote free radical polymerization or the ability of T^\bullet to recombine with I^\bullet or a polymer free radical segment including I^\bullet ; and

20 x and y are each integers of at least 1 and the sum of $x + y$ is not more than 12.

6. The copolymer of claim 1 further characterized by the representation by the formula



7. The copolymer of claim 1 further characterized by the selection of said iniferter from the group consisting of xylylene bis (N,N-diethyl dithiocarbamate) and xylylene bis (N-carbazolyl dithiocarbamate).

8. A sheet material further characterized by comprising the copolymer of claim 1.

9. A method of making a copolymer further characterized by comprising the steps:

35 (a) mixing (1) an iniferter represented by the general formula $I(T)_n$ capable upon being subjected to an appropriate energy source of forming free radicals $I(\bullet)_n$ and nT^\bullet wherein n is an integer of at least 2, I^\bullet is a highly reactive free radical capable of initiating free radical polymerization, and T^\bullet is a less reactive free radical which is generally much less capable of initiating free radical polymerization than I^\bullet but will rejoin with $I(\bullet)_n$ or a free radical polymer segment free radically polymerized with $I(\bullet)_n$ upon termination of
40 said energy source and (2) a first monomer charge selected from the group consisting of (i) acrylic monomer polymerizable to form an acrylic polymer block having a glass transition temperature of less than 0°C and (ii) monomer polymerizable to form a thermoplastic polymer block having a glass transition temperature of at least 50°C which is free radically polymerizable in the presence of $I(\bullet)_n$ to form a first polymer block;

45 (b) exposing the mixture of (a) to an energy source capable of forming free radicals $I(\bullet)_n$ and nT^\bullet ;

(c) maintaining the exposure of (b) until said first monomer charge polymerizes with $I(\bullet)_n$ to form a free radical polymer segment represented by the formula $I(B^\bullet)_n$ wherein B represents said first polymer block formed of said first monomer charge; (d) terminating said exposure whereby to cause $I(B^\bullet)_n$ and nT^\bullet to combine to form a polymer represented by the formula $I(BT)_n$;

50 (e) mixing $I(BT)_n$ with a second monomer charge which is the member of the group consisting of monomer (i) and monomer (ii) which was not selected as said first monomer comprising monomer which is free radically polymerizable in the presence of $I(B^\bullet)_n$ to a second polymer block;

(f) exposing $I(BT)_n$ to an energy source capable of forming free radicals $I(B^\bullet)_n$ and nT^\bullet ;

55 (g) maintaining the exposure of (f) until said second monomer charge polymerizes with $I(B^\bullet)_n$ to form a free radical block copolymer segment represented by the formula $I(BA^\bullet)_n$ wherein A represents said second polymer block formed of said second monomer charge; and

(h) terminating the exposure of (f) whereby $I(BA^\bullet)_n$ and nT^\bullet combine to form a block copolymer represented by the formula $I(BAT)_n$.

(19)



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(54) **Acrylic copolymers and method of making the same.**

(57) The present invention provides novel acrylic block copolymers and a method of making the same by use of an iniferter as a means of promoting, controlling and terminating polymerization. The method involves mixing an iniferter with a first polymer charge of acrylic monomer polymerizable to an acrylic block, exposing the mixture to an energy source to cause the iniferter to dissociate to form free radicals, permitting the first monomer charge to polymerize, terminating the exposure, adding a second monomer charge polymerizable to a second polymer block and again exposing the mixture to produce free radicals, permitting the second monomer charge to polymerize, and terminating the second exposure.

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DOCUMENTS CONSIDERED TO BE RELEVANT

Category	Citation of document with indication, where appropriate, of relevant passages	Relevant to claim	CLASSIFICATION OF THE APPLICATION (Int. Cl.5)
P,X	PATENT ABSTRACTS OF JAPAN, vol. 13, no. 151 (C-584)[3499], 12th April 1989; & JP-A-63 308 055 (MITSUBISHI PETROCHEM.) 15-12-1988 - - -	1-7	C 08 F 293/00
P,A	EP-A-0 286 376 (MITSUBISHI PETROCHEM.) * Examples 1,4,6; claims * - - - - -	1-9	
			TECHNICAL FIELDS SEARCHED (Int. Cl.5)
			C 08 F
The present search report has been drawn up for all claims			
Place of search		Date of completion of search	Examiner
The Hague		22 October 90	LOISELET-TAISNE S.M.
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